

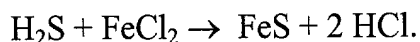
A METHOD FOR REDUCING HYDROGEN SULFIDE EMISSIONS FROM WASTEWATER

BACKGROUND OF THE INVENTION

[0001] The present invention relates to a method for reducing the dissolved sulfide content within a wastewater stream and thereby the hydrogen sulfide emissions there from and for improving water quality and treatment plant operations by employing a transition metal salt and an oxidant as additives to the wastewater stream.

[0002] Hydrogen sulfide (H₂S) is a toxic, corrosive gas that is generated within the biomass adhered to pipe walls and sediment of a sewage system. As wastewater is conveyed through the sewage collection system to the wastewater treatment plant, septic conditions develop that foster the growth of hydrogen sulfide-producing bacteria. Hydrogen sulfide volatilizes from the wastewater into the vapor space of the sewage system where it creates the problems of nuisance odors, infrastructure corrosion, and worker hazards.

[0003] The use of iron salts alone to control hydrogen sulfide emissions in wastewater is known in the industry. Iron salts control hydrogen sulfide (H₂S) by converting volatile H₂S dissolved in the wastewater into nonvolatile iron-complexed sulfide (FeS):



Ferrous sulfide (FeS) is a black precipitate that is stable in the absence of acid and typically settles out in clarifiers at the wastewater treatment plant, where it enters the solids stream. The stoichiometric chemical requirement is 1.7 pounds Fe (or 3.7 pounds FeCl₂) per pound H₂S controlled, yielding a cost of approximately \$0.50 per pound hydrogen sulfide depending on the per-unit chemical cost. Additionally the efficiency of iron salts is not impacted by oxygen uptake rates within the wastewater.

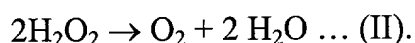
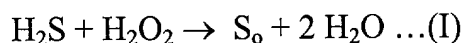
[0004] Despite these advantages, the use of iron salts alone to control H_2S emissions in wastewater has shortcomings. Iron salts alone lose efficiency when achieving H_2S emissions control for more than about four hours hydraulic retention time. Hydraulic retention time is defined as the length of time a component resides within the sewage system. Thus the efficient use of iron salts alone to control H_2S emissions of wastewater requires a series of iron salt injection facilities located along the course of the wastewater collection system. At each injection site, the spent iron salt (FeS) is augmented with fresh iron salt. As used herein, the term "iron salt" refers to nearly any iron compound (as distinguished from elemental iron) and expressly includes iron hydroxide ($Fe(OH)_2$, $Fe(OH)_3$, $FeCl_3$, $FeCl_2$, $FeSO_4$, and $Fe_2(SO_4)_3$) but excepts FeS , which is often referred to herein as "spent iron salt." The spent iron salt largely remains inert throughout the treatment and disposal processes. When the wastewater reaches the treatment plant, the mass of spent iron salt settles out in the primary clarifiers. The iron salt demand increases 2-4 fold to achieve H_2S emissions control for greater than about four hours hydraulic retention time, thus increasing the amount of spent iron salt generated. The FeS precipitates and constitutes a theoretical solids load of about 3 pounds per pound H_2S controlled. The FeS precipitate can cause deposition problems within the sewage system, particularly in low-velocity sewage systems and clarifiers/thickeners as it settles out, thus increasing the actual cost per pound H_2S controlled by 20% (\$0.075) or more.

[0005] Iron salts also degrade the quality of wastewater. The salinity of wastewater is increased by the addition of iron salts, as a minimum of 3 pounds sodium chloride per pound H_2S controlled is generated when $FeCl_2$ or $FeCl_3$ is used as the iron salt. Iron salts also deplete the alkalinity of the wastewater stream by consuming a minimum of 3 pounds calcium carbonate per pound H_2S controlled. Further, iron salt products typically contain 1-4% mineral acid that further depresses the pH of the wastewater. The reduced alkalinity of the wastewater stream in turn reduces the capturing capacity of iron, thus reducing its

ability to control H₂S to low levels. Furthermore, the depressed pH of the wastewater encourages volatilization of untreated H₂S within the wastewater stream. Additionally, iron salts deplete the wastewater stream of dissolved oxygen by consuming a minimum of 5 pounds dissolved oxygen per pound H₂S controlled. Thus, while iron salts are useful in controlling H₂S emissions of wastewater, it is desirable to minimize the amount of iron salt added to the wastewater stream to minimize the disadvantages associated with the use of iron salts.

[0006] It has been reported that a blend of 1 part ferrous to 2 parts ferric iron provides improved control of H₂S emissions from a wastewater stream when compared to either ferrous or ferric iron alone. Such a blend, however, is expensive and is subject to the same disadvantages of iron salts previously stated.

[0007] The use of hydrogen peroxide (H₂O₂) alone to control H₂S emissions is also conventional. Like iron salts, H₂O₂ injection facilities within the sewage system are typically located in series, separated by 1-2 hours hydraulic retention time. The use of hydrogen peroxide alone controls H₂S emissions in wastewater by two mechanisms: direct oxidation of H₂S to elemental sulfur (I) or prevention of H₂S formation by supplying dissolved oxygen (II):



Direct oxidation theoretically requires 1.0 pound H₂O₂ per pound H₂S controlled at a cost of about \$0.50 per pound H₂S and generates 1.0 pound solids per pound H₂S controlled, regardless of H₂O₂ dose. In contrast, prevention of H₂S formation by providing a dissolved oxygen supply theoretically requires 4.0 pounds H₂O₂ per pound H₂S controlled at a cost of \$2.00 per pound sulfide. The second mechanism also is adversely affected by environmental factors such as hydraulic retention time and oxygen uptake. Thus, the practical H₂O₂ requirement can be 2-4 times the theoretical H₂O₂ requirement when retention time increases by 2-3 hours. Therefore, previous H₂O₂ applications within the municipal wastewater treatment

industry are either targeted at point source H_2S control, such as at the headworks to treatment plants, where H_2O_2 may be applied to the wastewater stream to maximize its most efficient mode as an oxidant, or added as a preventative within the wastewater collection system, at costs exceeding \$2.00 per pound H_2S controlled.

[0008] While the independent use of H_2O_2 to control H_2S emissions by wastewater generates no adverse by-products and advantageously oxygenates the wastewater, it presents several shortcomings. Specifically, the oxidation reaction typically requires 15-30 minutes. In addition, control of H_2S emissions at 1-2 hours hydraulic retention time or more is expensive, requiring double the injection stations required by $FeCl_2$ control. Furthermore, the efficiency of H_2O_2 is adversely affected by high oxygen uptake rates. Hence, a mechanism which provides greater and more efficient H_2S emissions control within the wastewater treatment system is desirable.

[0009] In response to the need for an improved H_2S emission control mechanism, one study examined the effect of combining iron salt and sodium hypochlorite in a water treatment process. Specifically, sodium hypochlorite was added at the treatment plant to a force main discharge to which iron salt had been added at a pump station located upstream of the treatment plant. The results of the study demonstrated that such a combination treatment afforded more complete and consistent H_2S emissions control at reduced cost in comparison to the addition of iron salt alone to the waterstream. This process, however, has never been applied to a sewage collection system. Furthermore, this method of H_2S control has not been combined with a process for enhancing solids removal at the treatment plant.

[0010] A process for the conversion of aqueous hydrogen sulfide in geothermal steam employing hydrogen peroxide and iron compounds is taught by U.S. Patent No. 4,363,215 to Sharp. In the disclosed process, hydrogen sulfide is reacted with hydrogen peroxide, wherein the iron compound serves as a catalyst to accelerate the reaction of hydrogen peroxide with hydrogen sulfide. The iron compound

catalyst is added in an amount of from 0.5 to 1.0 parts per million expressed as free metal and thus does not complex with the sulfide. U.S. Patent No. 4,292,293 to Johnson et al. further discloses the addition of polyanionic dispersants to improve the efficiency of the metallic ion catalyst for the oxidation of sulfide by hydrogen peroxide.

[0011] The addition of a combination of a ferric salt and an anionic polymer to a water clarifier is a known development in enhancing solids separation and thereby improving the cost-performance of wastewater treatment plants, though such treatment has not yet been widely employed within the industry.

[0012] It is the object of the present invention to provide a cost-effective means for reducing hydrogen sulfide emissions throughout the wastewater collection system as well as the wastewater treatment plant while improving water quality and treatment plant operations.

BRIEF SUMMARY OF THE INVENTION

[0013] The present invention provides a novel method for integrating the use of transition metal salts and oxidants, specifically iron salts and hydrogen peroxide, respectively, to achieve reduced dissolved sulfide levels and thereby H_2S levels within a sewage system. Iron salts are added to the wastewater stream at the upper reaches of the wastewater collection system prior to H_2S volatilization to capture H_2S dissolved in the wastewater. The captured sulfide, as ferrous sulfide, is then delivered to one or more points downstream of the iron salt addition where hydrogen peroxide is added to the wastewater stream. The hydrogen peroxide destroys the ferrous sulfide and restores the sulfide-capturing capacity of the iron. At the final regeneration point, for example the wastewater treatment plant, the restored iron salt is used to enhance solids separation and sulfide control in primary clarifiers as well as sulfide and struvite control in anaerobic digesters.

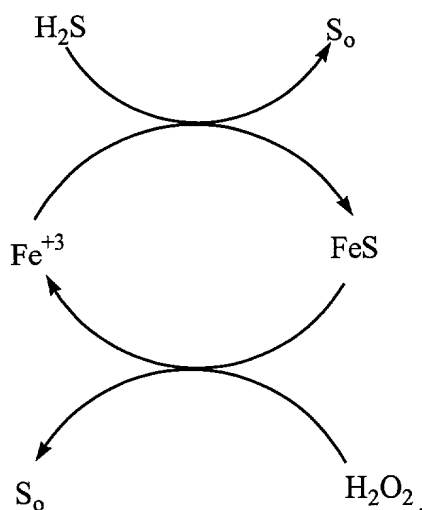
DETAILED DESCRIPTION OF THE INVENTION

[0014] Applicants have discovered a novel process for controlling hydrogen sulfide emissions from wastewater and for improving water quality and wastewater treatment plant operations in a cost-effective manner. The method of the present invention involves the use of transition metal salts to capture sulfides generated within a sewage system and to deliver the captured sulfides to an oxidant added at a point downstream of the transition metal salt addition. The oxidant restores the capturing capacity of the transition metal by regenerating a transition metal salt from the spent transition metal salt (transition metal sulfide), thus allowing the regenerated transition metal salt to participate in the capture of additional hydrogen sulfide molecules. The transition metal salt is preferably a ferrous or ferric salt in a solution or any readily water-soluble form. For example, the iron salt may be ferrous or ferric sulfate, chloride, nitrate, bromide, bromate, or a mixture thereof. The oxidant is preferably hydrogen peroxide.

[0015] The transition metal salt, preferably iron salt, is added to a wastewater stream at the upper reaches of a wastewater collection system prior to hydrogen sulfide volatilization. While hydrogen sulfide will begin volatilizing almost immediately, the term "prior to hydrogen sulfide volatilization" is intended to mean prior to *some* volatilization, not necessarily prior to *all* volatilization. The iron salt will aid in preventing future H₂S volatilization regardless of whether H₂S has volatilized previously. It would be practically impossible to introduce iron salt prior to all H₂S volatilization. The greater the amount of hydrogen sulfide already present in the wastewater stream at the point of iron salt addition, the greater the benefit of adding ferric salt to control hydrogen sulfide emissions, instead of ferrous salt, as ferric salt has an oxidizing capacity, albeit small. An oxidant, preferably hydrogen peroxide, is then added to the wastewater stream at one or more points downstream of the iron salt addition, to regenerate iron salt *in situ*. The hydrogen peroxide oxidizes the iron sulfide formed, to produce ferric hydroxide and/or ferrous hydroxide salts.

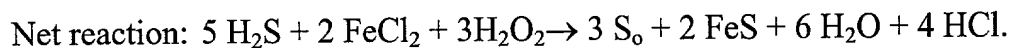
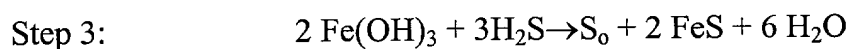
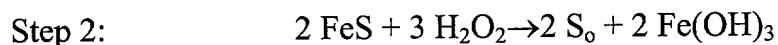
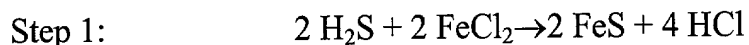
[0016] Multiple regeneration steps using a series of hydrogen peroxide additions spaced at points separated by approximately 4 hours hydraulic retention time may be used where the water collection system is long. In addition, hydrogen peroxide is preferably added to the influent wastewater stream at the wastewater treatment plant, the final regeneration point. The iron hydroxide produced enhances solids separation and sulfide control in primary clarifiers, as well as sulfide and struvite control in anaerobic digesters at the treatment plant. An anionic polyelectrolyte may be added to the influent of a primary clarifier at the wastewater treatment plant to further improve solids separation.

[0017] The present invention may be represented as the following catalytic cycle, where a working inventory of iron is maintained with hydrogen sulfide (H_2S) as the input, elemental sulfur (S_0) as the output, and hydrogen peroxide (H_2O_2) as the driver:



The preferred embodiment of the process occurs in three steps: (1) iron complexation with dissolved sulfide; (2) direct H_2O_2 oxidation of the FeS complex to provide elemental sulfur and ferric hydroxide ($\text{Fe}(\text{OH})_3$); and (3) oxidation of additional sulfide by the ferric hydroxide to produce elemental sulfur and FeS . The second and third steps are then repeated as additional hydrogen peroxide is

used to regenerate ferric hydroxide from the ferrous sulfide. The preferred process may be exemplified in the following overall reaction:



This net reaction stoichiometrically requires 0.67 lbs Fe (or 1.45 lbs FeCl₂) and 0.6 lbs H₂O₂ per lb sulfide, to yield a theoretical cost of about \$0.50 per lb sulfide controlled. This is based on 0.67 lbs Fe²⁺. Commensurately less iron would be required if introduced as Fe³⁺. In that case, only 0.5 lbs Fe³⁺ and 0.6 lbs H₂O₂ per lb sulfide controlled would be needed.

[0018] The method of the present invention achieves a number of advantages over conventional methods. In sharp contrast to conventional treatment techniques the addition of fresh iron salt downstream of the initial injection site or even at the treatment plant is not required, as a mixture of ferric and ferrous salts is provided by *in situ* regeneration of spent iron salt by hydrogen peroxide in the wastewater collection system and upon entry of the treatment plant. Because iron salt need only be added to the wastewater stream at one point in the collection process and is regenerated thereafter by hydrogen peroxide, the present invention requires only a fraction of the iron input required by the related art. Thus, the present invention achieves a greater than 40% reduction in solids production, a greater than 60% reduction in acidity contribution, and a greater than 80% reduction in dissolved oxygen demand. These benefits result in an overall cost savings by reducing the solids load and the amount of iron salt required, thus reducing the solids generated and associated disposal cost.

[0019] Additionally, the iron levels in the wastewater stream augmented by reaction of FeS with H₂O₂ increases the removal rate of H₂S by more than 90%, thus significantly improving the degree of H₂S control afforded as compared to the

use of iron salt or H_2O_2 alone. For example, the use of H_2O_2 alone to control sulfide emissions requires H_2O_2 addition at a site 20-40 minutes hydraulic retention time upstream of the point of H_2S release. In sharp contrast, the present invention allows the addition of H_2O_2 to be located at or 1-10 minutes prior to the point of desired H_2S control.

[0020] Regeneration of iron salt with H_2O_2 also results in a mixture of ferric and ferrous salts having superior H_2S capturing capacity as compared to ferric or ferrous salt alone. The ferrous-to-ferric iron ratio of this blended product may be adjusted by varying the H_2O_2 dose.

[0021] The present invention represents a novel and significant improvement for reducing H_2S emissions from wastewater. In addition to providing practical, long-duration H_2S control to low sulfide levels via a rapid oxidative reaction, the method of the present invention provides significant treatment plant benefits. The invention being thus described, it will be obvious that the same may be varied in many ways. Such variations are not to be regarded as a departure from the spirit and scope of the invention, and all such modifications as would be obvious to one skilled in the art are intended to be included within the scope of the following claims.